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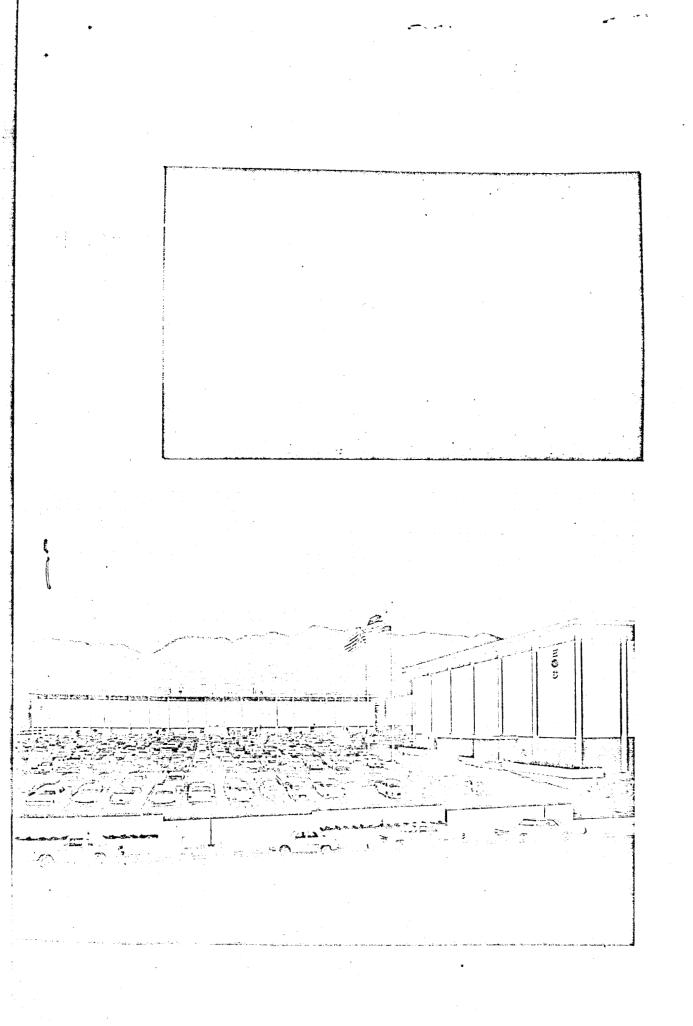
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HYDROGEN-ONYGHE ELECTROLYTIC REGENERATIVE TUEL CHLES

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ELECTRO-OPTICAL SYSTEMS, INC.

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SECTION 1

INTRODUCTION

This report reviews the progress made on the development of a hydrogen-oxygen ($\rm H_2-\rm O_2$) regenerative fuel cell (secondary battery) under MASA Contract MAS3-2781 during the period 1 May 1967 through 1 June 1967. During this period, primary emphasis was placed on the testing of single cells with matrix structures of potassium titanate and teflon. Reference cells were assembled and tested. A six-cell unit was tested. Fabrication has begun on the 28-volt 500-watt Flight Prototype Fuel Cell assembly.

SECTION 2

TECHNICAL DISCUSSION

2.1 SINGLE CELL TESTS

Eight single cell tests were conducted during this period to evaluate matrix and electrode configurations. Test results and construction variables of these cells are summarized in Table I.

2.1.1 SINGLE CELL MATRIX TESTING

A 35-mil KT and teflon composite membrane was fabricated using the same techniques used in cells 262 and 264 then sandwiched between two 35-mil KT-asbestos mats. This matrix contained 65 gm of 39.7 percent KOH and was installed with a 60-mil spacer in cell 266. The cell contained the usual EOS-American Cyanamid electrodes. The cell has run a total of 745 cycles and the test has been discontinued. As can be seen in Fig. 1, the performance was good, above 0.7 volts on discharge, for over 600 cycles and the degradation was slow. After cycle 660 the degradation in performance was more obvious. Testing was discontinued after 745 cycles. Upon disassembly it was observed that part of the ET-teflon composite membrane had lost its latex property and appeared to have become hard, densely packed particles forming a structure like a porous brick. A KOH analysis showed a final concentration of 35 percent MOF. The degralation in performance may have been caused by the asbestos present in the mats. The electrolyte consumption was too small to affect performance. Dissolved asbestos in the catalyst reaction sites might be a factor. This cell, however, did not contain an optimum electrolyte matrix spacing arrangement and the performance may have been affected by a gradual displacement of electrolyte.

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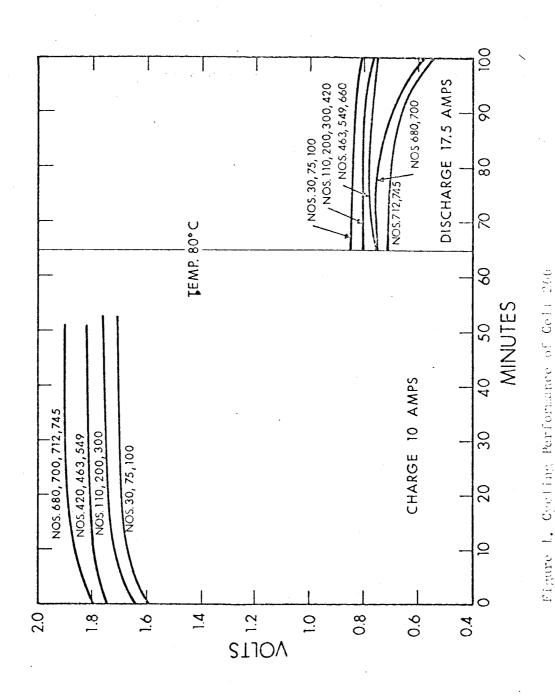
TABLE I SUPPLARY OF SINGLE CELL TESTS

Comments	Reverse current cycling Hz sas concentration cell. Cell has run #1228 cycles. Test still in progress. Test temperature 80°C.	Test discontinued after 746 cycles. performance good until cycle 660 where the degradation became extreme Test temperature 80°C Final KOH 35%	Cell has run 396 cycles performance excellent. Test still in progress.	Reference cell. After total two cycles fast self discharge.
Spacer (inch)	090.0	090.0	090.0	0.060
Flectrolyte	40.0g of 39.7% kom	65g of 40% KOII	56.1g of 40% KOH	40g of
Matrix	50/50 KT and teflon pasted membrane sandwiched between 2-90/10 KT and AD mats	80/20 KT and teflon composite membrane sandwiched between 2-90/10 KT and AB mats	A 50% KT/50% teflon membrane sandviched between two 80% KT/20% teflon rolled composites	50/50 KT and teflon pasted membrane sandwiched 2-90/10 KT and AB mats
Electrodes	N2 EOS O2 EOS Both new and treated for one hour in 40% KOH	Ng EOS Og Cyanamid Both used in run #264	N2 EOS O2 Cyanamid Both used in run #254	112 EOS O2 Cyanamid New electrodes
Cell	265	992	269	271

TABLE I

SUMMARY OF SINGLE CELL TESTS (contd)

Comments	Reference cell. After total three fast self discharge.	Reference cell. After total 31 cycles fast self discharge.	Cell has run 292 cycles and shows excellent performance. Test still in progress.	Reference cell performance good up through cycle #43. Cycle #44 cell began to self discharge.
Spacer (inch)	090.0	090.0	0.050	090.0
Spacer Flectrolyte (inch)	40g of	40g of 40.3% kom	47.0g of	45.3g of 40.3% kon
Matrix	50/50 KT and teflon pasted membrane sandwiched 2-90/10 KT and AB mats	50/50 KT and teflon pasted membrane sandwiched between 2-90/10 KT and AB mats	Pressed KT-Asbestos teflon composite 0.060" thick	50/50 KT and teflon pasted membrane is sandwiched between 2-90/10 KT and AB mats
Electrodes	Hy EOS O, Cyanamid Both used in runs #263 and 270	N2 EOS O ₂ Cyanamid New Electrodes	11, FOS 0, Cyanamid Both used in runs #263, 270 and 272	H ₂ EOS O ₂ Cyanamid Doth used in runs #272 and 273
Ce 11	27.2	273	274	275



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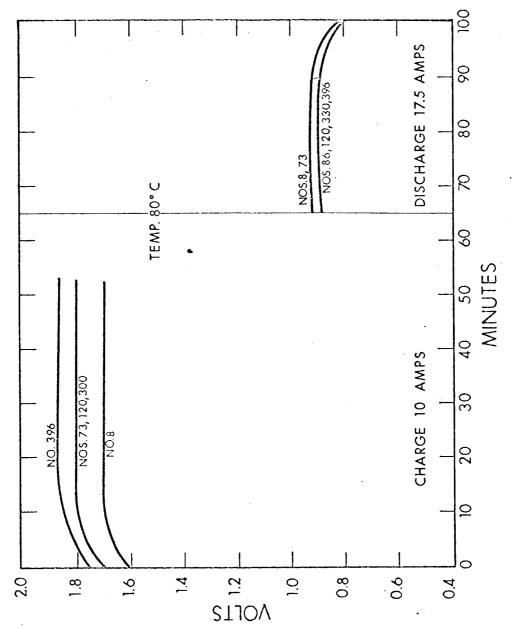
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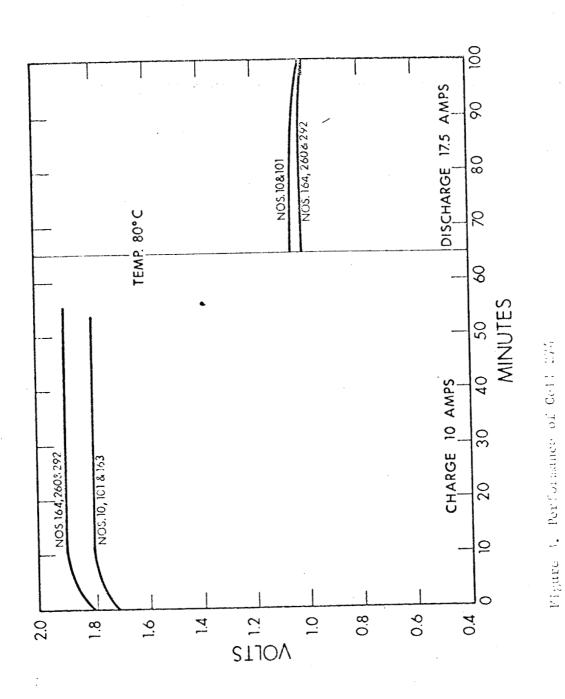
A matrix was made by forming a rolled 0.030 IT-teflor composite on each side of a membrane (50 percent KT-50 percent teflor pasted on 100 mesh screen). The matrix was assembled in cell 269 with a 0.060 spacer and 56.1 gm of 40 percent KOH. Both the EOS and Cyanamid electrodes were used in a previous cell. The cell has run 396 cycles to date and the performance is excellent, above 0.85 volts. As can be seen in Fig. 2 there has been little degradation in performance. The test is still in progress.

A pressed composite matrix was fabricated with KT, asbestos and teflon and successfully lab tosted. Another matrix 0.060 inch thick was fabricated. It was assembled in cell No. 274 with 47.0 gm of 40.3 percent KOH electrolyte and a 0.050 inch spacer. The EOS Cyanamid electrodes have been used in previous cells. The cell has run a total of 292 cycles and is still cycling. Figure 3 shows that to date the performance has been most excellent, 0.9 volts and above. The degradation has been slight. The performance may have been helped by the closer spacing, 0.050 inch.

2.1.2 H₂ CONCENTRATION CELL

Cell 265 is a cycling hydrogen concentration cell. It contains two EOS $\rm H_2$ electrodes and has a 50 percent KT-50 percent tellon membrane sandwiched between two 90 percent KT-10 percent ashestos mats. All the KT was treated in $100^{\circ}\rm C$ KOH for one hour and washed with distilled H₂O. The matrix contains 40 gm of 39.7 percent KOH. A 60-mil spacer is being used. The cell was flushed with H₂ gas then 150 psi of H₂ was introduced. A cycle of 18 amp charge for 35 minutes was set up. The cell has run 1228 cycles to date, and is still running. Figure 4 shows the performance. The voltage has slowly risen to 0.325 volts and may stabilize.





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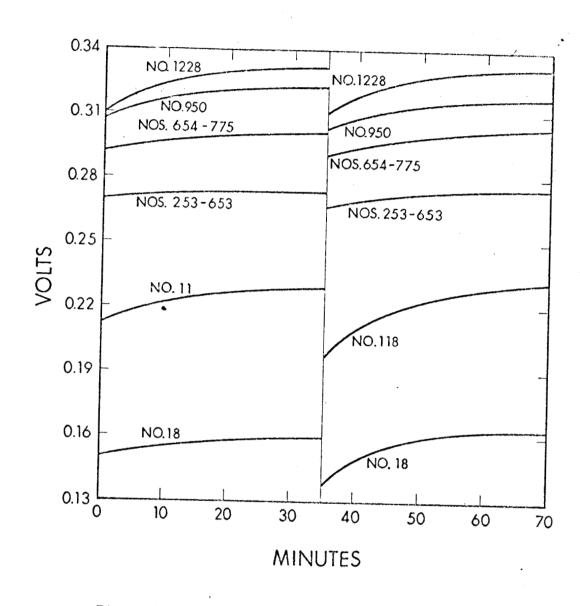


Figure 4. Cycling Performance of H_2 Concentration Cell 265

2.1.3 REFERENCE CELLS

In order to characterize the American Cyanamid and EOS electrodes used in the EOS fuel cell, reference cell testing is being continued. Cell 271 contained an AB6 American Cyanamid oxygen electrode and a standard EOS electrode (of 20 mg Pt/cm²). The matrix was made of a pasted KT-teflon membrane sandwiched between two 90 percent KT and 10 percent asbestos mats. On each side of the membrane was placed a mercuric oxide (NgC) reference electrode. The reference electrodes consisted of nickel screens on which NgO powder was pressed. Each screen had a nickel wire spot welded on one end; the wire was fed out through the 60-mil insulating spacer. Reference cell 271 ran two cycles then began to self discharge. The cause could not be determined by visual inspection.

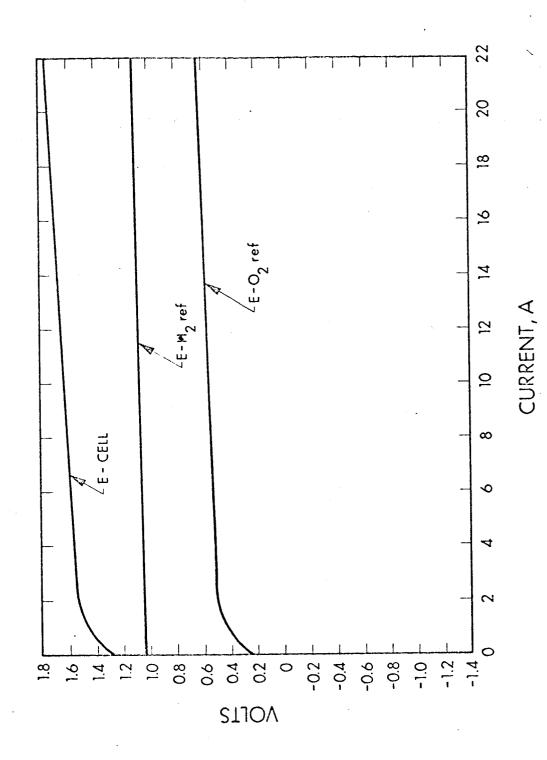
Another reference cell, No. 272, was built in the same manner as above and failed in like manner.

Reference cell No. 273 was built in the same manner as above. This cell ran 30 cycles before it failed to hold a charge. Figures 5 and 6 show the charge and discharge polarization curves for this cell.

These curves are typical when compared to previous reference cell data.

Another reference cell, No. 275, was built in the same manner as above. This cell performed for 43 cycles before it failed to retain a charge.

Since this type of matrix arrangement has successfully demonstrated long cycle life without cross gas leahage in regular cycling tests, the inclusion of the reference electrode must be causing the cross gas leahage. This may result from the depressions caused by the reference wires which are fed into the cell through the matrix. In the future, attempts will be made to use thinner wires.



gare 5. Charge Polarization of Reference Cell 273

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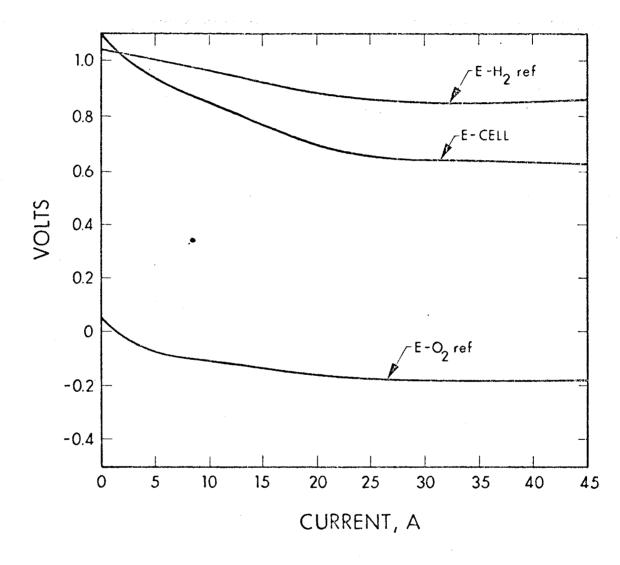


Figure (. Discharge Polarization of Reference Cell 2.)

2.2 SIX CELL TESTING

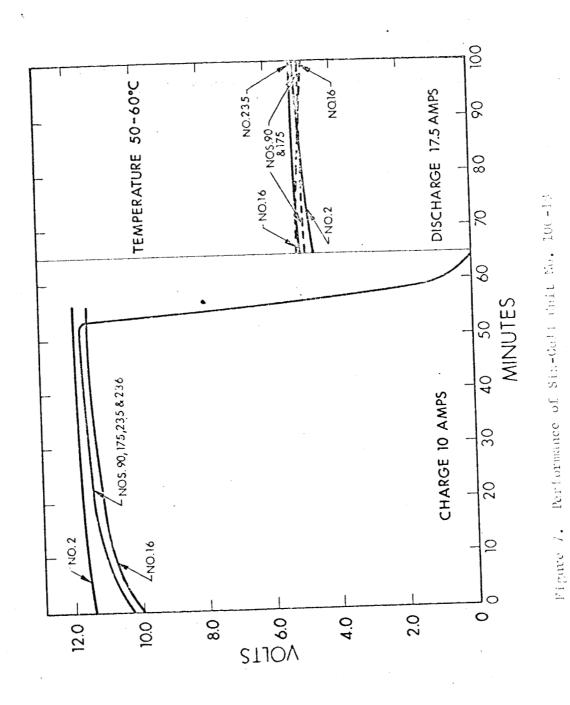
A six cell unit, No. 100-13, was assembled during the last report period. The $^{\rm O}_2$ electrodes were American Cyanamid AB-6 type, and the H $_2$ electrodes were EOS 25 mg Pt/cm 2 carbonyl nickel plaques. The matrixes consisted of 50 percent KT-50 percent teflon pasted membrane sandwiched between two 90 percent KT-10 percent ashestos mats. Forty gm of 40 percent KOH was added to the matrixes and 60-mil spacers were used.

As can be seen in Fig. 7, the cell ran well with no degradation for 235 cycles. Near the end of charge at cycle 236 the cell pressure rose from 350 psi to 450 psi in less than a second. The cell voltage rapidly fell to zero. When taken apart, it was evident the cell stack was damaged by an extremely fast recombination of the gases. Upon inspection the cause of failure was found in the H₂ end plate. As can be seen in Fig. 8, a photograph of the end plate, at the spot the arrow indicates the inside scaling edge of the plate is warped approximate. The warpage is a swelling caused by the formation of magnesium exide from exposed magnesium and KOH. The swelling forced the end plate and bipolar plate apart, eventually allowing the gases to rapidly mix and recombine. This plate had been previously used and reworked by patching holes in the nickel plate with silver epoxy, then plating gold over the patch.

Figure 8 shows that not one of the patches held and corrosion occurred at all the spots repaired. Another six-cell unit will be built and tested as soon as new hardware is obtained.

2.3 MATRIX FABRICATION AND SCREENING

Fabrication of composite matrixes using KT, asbestos and teflon pressed together was explored during this period. Table II summarizes the



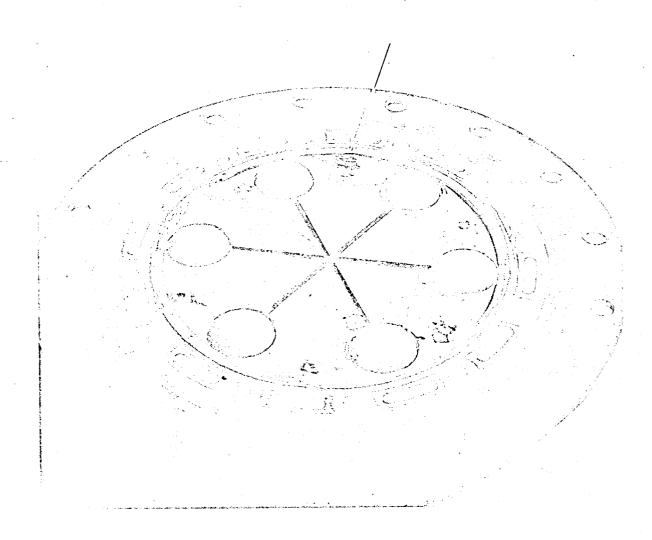


Figure 8. H_2 End Plate From Six-Cell Unit No. 100-13

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Thickness (dry) mils	76	34	. 67	145
Thickness (wet) mils	12 2 15 15 15 15 15 15 15 15 15 15 15 15 15	82 20 15 8	81 71 71 61 61	148 120 100 98 88
Com- pression	213 213	213 355 390	0 160 284 390 710 850	178 213 223 284 284
Resistance	0.136 0.126 0.116 0.096	0.137 0.117 0.102 0.097	0.167 0.117 0.097 0.087 0.072	0.137 0.137 0.127 0.117 0.112
Resistivity	32.4 46.8 40.8 37.4	77 105 122 218	37.0 27.7 24.6 23.7 25.2	16.5 19.3 19.4 20.5 32.7
Bubble- through	15	ιζ	20	10
Composition	Sandwich two 90/10 KT and asbestos mats, 50/50 KT and teflon 100 mesh screen membrane between mats pressed	90/10 KT and asbestos mat pressed at hour 124 psi	Matrix consisting of 82% KT, 10% asbestos and 8% teflon pressed at % hour 124 psi	Matrix consisting of 83.5% IT ,8.25% asbestos 8.25% teflon not pressed
Sample		N-2	£-1-3	77-77

screening test results. Sample M-1 is the standard sandwiched matrix used in many of the current tests. Sample M-2 is a standard 90 percent KT/10 percent teflon matrix. The bubble-through pressure of 15 psi for the matrix (M-1) and 5 psi for the mat (M-2) along with the respective resistivity data give a baseline to compare the new structures with. Samples M-3 and M-4 are the MT, asbestos, teflon composites. The variable in fabrication is that sample M-4 was unpressed. The pressed matrix demonstrated the superior bubble through test of 20 psi. The unpressed matrix gave a result of 10 psi which is below that of the sandwiched matrix but better than the pressed MT/asbestos, mat (M-2). A pressed matrix similar to sample M-3 is currently being used in cell No. 274 with excellent results.

2.4 PLATINY AVAINSTS OF CONCERTRATION CELLS

To determine whether platinum migration occurs by some soluble form into the matrix where it is reduced by hydrogen, the following test was performed on cells No. 252, 257 and 260. The cells were flushed with 0_2 gas, then 150 psi of 0_2 gas was introduced. A cycle of 18 amps forward charge for 35 minutes and 18 amps reverse charge for 35 minutes was set up. At the end of 57 cycles the cell was shut down and purged with $\rm H_2$ gas. 150 psi of $\rm H_2$ gas was added to the cell and it was left on stand for 24 hours. At the end of this period the cell was disassembled and the membrane analysed for platinum. The results are as follows:

Cell	252	0.115 mg Pt/cm ²
Cell	257	$0.0088 \text{ mg Pt/cm}^2$
Cell	260	0.0036 mg Pt/cm ²

The results show a definite transfer of platinum. The reverse cycling in the O_2 concentration mode is extreme and may not represent what is

occurring in a functioning fuel cell. Additional platinum analysis will be done on the longer life cells in order to establish a quantitative basis to evaluate this problem.

SECTION 3

PLANS FOR THE NEXT PERIOD

Single-cell cycling tests and lab screening will be continued to evaluate KT matrixes of different total weight, electrolyte-to-matrix weight ratios, thicknesses, compression ratios, and additions of asbestes teflon, polypropylene, and other fibers that can improve the structure of the matrix. Another reference cell will be assembled and cycled. Fabrication of the 34 cell unit will continue.